

## **AMENDMENTS TO THE CLAIMS:**

Please amend the claims as follows:

1. (Original) An elimination process of fluorinated anionic surfactants from exhausted gaseous streams wherein the gaseous stream is put into contact with aqueous solutions having pH from 3.5 to 13.8, the aqueous solution density being lower than  $1.05 \text{ g/cm}^3$ , preferably lower than  $1.03 \text{ g/cm}^3$ , wherein the concentration in the aqueous solution of the fluorinated anionic surfactant removed from the gaseous stream is lower than or equal to 70 ppm, preferably lower than or equal to 60 ppm, still more preferably lower than 50 ppm.
2. (Original) A process according to claim 1, wherein the anionic fluorinated surfactants are selected from perfluorinated carboxylic acids or derivatives thereof, preferably perfluorooctanoate in acid or salified form.
3. (Currently Amended) A process according to ~~claims 1-4~~ claim 1, wherein the contact between the gaseous stream and the aqueous solutions is carried out in a scrubber.
4. (Original) A process according to claim 3, wherein the used absorption column is a filling up column, preferably structured, a plate column or a spray column; preferably a spray column is used.
5. (Currently Amended) A process according to ~~claims 1-4~~ claim 1, wherein one operates in a discontinuous or a continuous way, preferably in a continuous way.
6. (Original) A process according to claim 5, wherein one operates in a continuous way according to one of the following methods:

- by recycling the solution and recovering the surfactant at each recycle,
  - by recycling the solution until reaching a surfactant concentration of 70 ppm and then by treating the liquid phase to remove the surfactant,
  - by using in the gas absorption phase fresh solution without recycle,
  - by feeding a fresh aqueous solution aliquot and drawing from the plant an aliquot containing the anionic surfactants to be sent to a recovery plant.
7. (Original) A process according to claim 5, wherein when one operates in a discontinuous way, the solution used in the absorption column is recycled until a surfactant concentration of 70 ppm is reached.
8. (Currently Amended) A process according to ~~claims 1-7~~ claim 1, wherein the surfactant is recovered from the aqueous solution flowing out from the absorption column by one of the following methods:
- by passing the solution on anionic exchange resins,
  - by using specific adsorbers for fluorinated surfactants,
  - by reverse osmosis units,
  - by precipitation with polyvalent cation salts.
9. (Original) A process according to claim 8, wherein a strong anionic exchange resin is used.
10. (Original) A process according to claim 8, wherein the used specific adsorbers are selected from active carbon, aluminas, silicas.

11. (Currently Amended) A process according to ~~claims 1-10~~ claim 1, wherein the initial removal solution, and/or the recycle solution have a temperature in the range 5°C-40°C preferably 10°C-30°C.
12. (Currently Amended) A process according to ~~claims 1-11~~ claim 1, wherein in the scrubber the ratio by weight among the flow rates of the feeding aqueous solution and fed gas is from 2 to 20, preferably from 4 to 15.